

550 N. 31st Street, Ste. 500 P.O. Box 7168 Billings, MT 59101

May 20, 2014

NSR Program Manager/Attn: O&G Production Facilities Wyoming Dept. of Environmental Quality Air Quality Division Herschler Bldg., 2-E 122 West 25th St Cheyenne, WY 82002



Re: Permit Applications for Roger Leo Fed 3875-20-29-1FH and Spearhead Fed 14-7H

Dear Permitting Engineer:

SM Energy Company respectfully submits the following permit applications for the Roger Leo Fed and the Spearhead Fed. Both of the permit applications were submitted electronically and this envelope includes the additional paper copy with original signature.

Please contact us with any questions or concerns.

Respectfully,

Luke Studer

SM Energy Company

Reviewer HMB

cc:

Modeler

D.E.

File Accol 133

IMP FID FO26612

Roger LEO



Department of Environmental Qual

Permit Application Forn

s this a revision to an existir	ng application?	
Yes	No X	
Previous Application #:		

65	32425262778	200
255	*	
83	MAY 2015	
8	RECEIVED	2
ity Air Qu	IAIITY DIVISION	I A
n E	DISIOIA	03
1	831110168	L'ST
	211010	

	Yes	= 1	No	Х	en.	Date of Application	n:5/21/201
	Previous Appli	cation #:					
COMPANY INFO					= =		
Company Name:				SM Energ	v Co.		
Address:		550 No	orth 31st 9	Street Suite 5			TOTAL T
City: Billi	ngs	State:		ntana		Zip Code	= 59103
Country:	USA			ne Number:	l.	4068698706	
FACILITY INFORM	/IATION:			1971 11	THE PERSON NAMED IN		
Facility Name:	581		Roger I	eo Federal 3	875-20-29-1FH	little from the pro-	
New Facility or Existin	g Facility:	New			Direct Contract Contr		
Facility Description:			Oil a	nd Gas Produ	iction Facility		
Facility Class:	Minor			ating Status:			
Facility Type:	Pro	oduction Site					
	681						
For Oil & Gas Product	ion Sites ONLY	:					
irst Date of Producti			on:	April 2, 2015	<u> </u>		
Does production at the		ain H2S?*	[No			
*If yes, contact the D	ivision.				a again an an Life		
API Number(s):				49-00	09-29320		
NAICS Code:		21	1111 Cru	de Petroleun	n and Natural G	Cas Extraction	
FACILITY LOCATION	ON		.IIII Ciu	de l'etroieuri	ir ariu ivaturar c	Jas Extraction	
		******************************	. 51.10 14.		, -	adama a per	
Enter the facility location hysical Address:	on in either the ia	titude/iongitude	area or sec	tion/township)/range area. Bo	th are not required.	
City:		71	o Code:				
State: WY		County:	o coue.				
		county.					
<u>OR</u>						2	
_atitude:43.25	5716	Longitude:	-105.	88214		County	/: Converse
Quarter Quarter:	NE		Quarter:		NE	/	·
Section: 20		Township:		BN		Range	
For longitude	and latitude, u	se NAD 83/WG	S84 datu	m and 5 digi	ts after the dec	cimal (i.e. 41.12345,	-107.56789)
CONTACT INFOR	MATION:					V	
Note that an Environmental	AND NSR Permitting	Contact is required	for your app	ication to be dee	med complete by th	ne agency.	
Title: Mr.		First Name:			Luke		
ast Name:	J	Studer					_
Company Name:				SM Energ	v Co		
Job Title:			Sr. F	H&S Specialis			
Address:	4	51		31st Street S			
	Billings		ate:		Montai	na	T
Zip Code: 59103	2.111165		u.c. [iviorital	IU	_
Primary Phone No.:	406-869	 0-8706		E-mail:		lstuder@sm-energy	com
Mobile Phone No.:				Fax No.:		istude wsiii-effergy	.com
Contact Type:	Environmen	tal contact		Start Date:			
Jonitall Type.	LIMITOTITIET	tai contact		Start Date.			

Additional Contact Ty	pe (if needed): NSR	Permittin	g contact	1	
Title: Ms.	First Name:	April 1990 Marie San Carlo		Lynn	
Last Name:	Olson				
Company Name:			— Trihydr	о Со	
Job Title:			Air Scientist		
Address:		28769	Edward View	Drive	
City:	lighland	State:		California	
Zip Code: 92346					
Primary Phone No.:	(307) 633-9506		E-mail:	lolson@trihydro.com	
Mobile Phone No.:			Fax No.:		
Contact Type:	NSR Permitting contact		Start Date:		
FACILITY APPLICA	ATION INFORMATION	:			
General Info:					
	ed location or is it a new/ gr	eenfield fa	cility?		Yes
	ng document been included				No
	n a sage grouse core area?*				No
	ge grouse core area, what is		number?		
	sage grouse core area, cont			partment.	
	plicability - Facility Le				
	int Deterioration (PSD):	vci.			No
Non-Attainment New					No
					140
Modeling Section				t d2	No
AND SECURITY OF THE PROPERTY O	vision been contacted to det	ermine it i	modeling is re	quirea?	No No
is a modeling analysis	part of this application?				INO
Is the proposed project	t subject to Prevention of S	ignificant [Deterioration	(PSD) requirements?	No
	rision been notified to sched				No
	col been submitted to and a				No
	rision received a Q/D analys				
the need for an AQRV					No
Required Attachr	Herocoleccus of the let				
Facility Map	Hents.	L	7		
Process Flow Diagram		Г	_ 		
Modeling Analysis (if a	nnlicable)	_	=		
Land Use Planning Doo		F	1		
Detailed Project Descr			_ 		
Emissions Calculations					
LITII3310113 Calculations		_	_		
1	Luke Studer			Sr. EH&S S	Specialist
.,	Responsible Official (Prin	ted Name)	Tit	
		•			
an Official Representa	tive of the Company, state t	hat I have	knowledge of	the facts herein set forth	and that the same
	the best of my knowledge				
	ed on this application reflec				
	compliance with all applical				
**************************************	. n	0.			
	1				
Signature:	10			Date	:

Company Name	SM Energy	
Facility Name	Roger Leo Federal	

Process Description

The Roger Leo Federal 3875-20-29-1FH is powered by a generator (previously permitted: P0005290) to run the pumping unit and facility.

The fluid stream containing natural gas, crude oil and produced water is routed to the vertical treater. The treater has a 0.75 MMBtu/hr heater. Three streams are generated in the treater including gas, oil, and water.

The crude oil stream is sent to one of the eight oil tanks. The tank vapor emissions are captured and sent to the low pressure tip of the Steffes flare (on-site). The combustion efficiency is estimated at 98 percent. The crude oil is hauled offsite by tank trucks.

The gas phase stream leaves the separator and is sent offsite to a pipeline owned by a third party. The stream is also used to fuel the vertical treaters burner if additional fuel is needed. If the gas cannot be sent to the sales line, it will be sent to the high pressure tip of the Steffes flare (considered an emergency situation).

The water is sent to two 400-barrel aboveground storage tanks and sent off site by truck. Since little water is produced and the water is from a treated stream, emissions are assumed to be minimal.

Fugitive emissions are associated with the valves, gauges, tank vents, hatches and connectors at the site. The components were estimated based on similar facilities. An exact component count was not performed.

STATE OF WYOMING



Department of Environmental Quality - Air Quality Division Oil and Gas Production Facilities C6 S2 Permit Application



Equipment List

Company Name	SM Energy
Facility Name	Roger Leo Federal
produced water storage tanks, a control equipment and devices. atmosphere during times other t gun barrels, scrubber pots, etc). Provide size of production & wa	the site including all pressurized vessels with the potential for flash emissions, all hydrocarbon liquids and all dehydration units, all pneumatic pumps, all natural gas-fired burners and heaters and all emission. Pressurized vessels with the potential for flash emissions are all vessels that vent vapors to the than upset or emergency conditions (water knockouts, 2-phase and 3-phase separators, heater treaters, Provide design ratings for dehys (MMCFD), process heaters, burners and pilots (MMBtu/hr, SCFH). ter storage tanks (BPD). For dehydration units indicate if the unit includes a glycol flash separator and/or or emission control combustors/flares indicate design rating (MMBtu/hr, SCFD) and combustor/flare height notive gas usage (SCFH).
2 400-bbl water tank	
8 400-bbl oil tanks (control	
1 6' x 20' vertical treater wit	
1 rotaflex pump with assoc	siated generator (already permitted: P0005290) with a low pressure tip for tank vapors and higher pressure for emergencies when
produced gas cannot go to	
produced gas cannot go to	Guico IIIIC
	x
FORM AQD-OG2 Equipmen	nt List AUGUST 2007

Heater/Chiller

Company Equipment II	D: Roger Fed	d Heater Treater heater			
Company Equipment D	escription:	Heater Treater heater			
					Shar en in
Operating Status:	Operating	Take Take	Total City	nik Vermon	
Initial Construction Commencement Date:		Oct 2014 - F	Feb 2015		
Initial Operation Comm		4/2/3	15	2.65.00	dajilare i mir e e si
Most Recent Construct					50
Commencement Date:		NA	\		The state of the s
Most Recent Operation	n Commencement Date	e: NA	1		
Select reason(s) for thi	is emissions unit being	included in this application	on (must b	e comple	ted regardless of date
of installation or modi			•	L. i lfic	I I aga Bac I I bea
Reason	: Construction (Greenf	ield/New Facility)			
If reason is <i>Reconstruc</i>	tion or Temporary Per	mit or Other, please expla	ain below:	A pp	
Firing Type:	Direct		D D		
Heat Input Rating:	0.75	U	Jnits:	MMBtu/	hr
Primary Fuel Type:	Field Gas				
Secondary Fuel Type:					
Heat Content of Fuel:	1270	sent australium in the Tri		Units:	BTU/scf
Fuel Sulfur Content:	0	U	Jnits:	ppm	
SCC Codes: List all Sour source (e.g., 1-02-002-0		s) (SCC) that describe the p 2310010100	orocess(es) perform	ed by the emission
Potential Operating So	chedule: Provide th	ne operating schedule for t	his emissi	on unit.	
Hours/day:	24				
Hours/year	8760				

Control Equipment: If yes, please fill out o	No and attach the appropriat	te Control De	evice and Release Po	int Informati	on worksheets.
Best Available Contro	ol Technology (BACT): Wa	as a BACT An	alysis completed for	this emission	unit?
Yes		No	X		
Pollutant:					
Proposed BACT:					
*If yes, attach BACT A	nalysis with this application	on.			
Lowest Achievable En Yes Pollutant:	nission Rate (LAER): Was		lysis completed for th X	iis emission u	nit?
Proposed LAER:					
AND THE RESIDENCE OF THE PROPERTY OF THE PROPE	nalysis with this application	on.			
New Sour	ance Standards (NSPS): ce Performance Standard c of Performance for New S	are listed un			
National Emission Sta	ndards for Hazardous Air	Pollutants (N	NESHAP Part 61):		Not Affected
61. (These	Emissions Standards for He e include asbestos, benzel ESHAP Subpart:				listed under 40 CFR
National Emission Sta	ndards for Hazardous Air	Pollutants (N	IESHAP Part 63):		Not Affected
standards	Emission Standards for Ha are listed under 40 CFR 6 ESHAP Subpart:		Pollutants (NESHAP i	Part 63)	
	ant Deterioration (PSD): es are found under WAQS		Not Affected , Section 4.		
Non-Attainment New	Source Review: es are found under WAQS	Not Affecte R Chapter 6			

Emissions Information- The following tables request information needed to determine the applicable requirements and the compliance status of this emission unit with those requirements.

Efficiency Standards Pre-Controlled Potential Potential to Emit to Emit Potential Emissions to Emit Basis for (PTE) (lbs/hr) (tons/yr) (tons/yr) Units Determination Criteria Pollutants: 1.) Particulate emissions (PE/PM) (formerly particulate matter, PM) 2.) PM #10 microns in diameter (PE/PM10) 3.) PM #2.5 microns in diameter (PE/PM2.5) Sulfur dioxide (SO2) 0.0006 lb/MMBtu 0.0004 0.0019 AP-42 5.) Nitrogen Oxides (NOx) lb/MMBtu 0.10 0.07 0.32 AP-42 6.) Carbon monoxide (CO) 0.08 lb/MMBtu 0.06 0.27 AP-42 7.) Volatile organic compounds (VOC) 0.01 lb/MMBtu 0.00 0.02 AP-42 8.) Lead (Pb) 9.) Total Hazardous Air See Pollutants (HAPs) attached 0.00 0.01 AP-42 10.) Fluoride (F) 11.) Hydrogen Sulfide (H2S) 12.) Mercury (Hg) 13.) Total Reduced Sulfur (TRS) 14.) Sulfuric Acid Mist (SAM)

^{*}Provide your calculations as an attachment and explain how all process variables and emissions factors were selected.

Hazardous Air Pollutants (HAPs) and Toxic Air Contaminants

			Effic	ciency Standards			
		Pre-Controlled	Potential		Potential	Potential	
		Potential Emissions	to Emit		to Emit	to Emit	Basis for
		(tons/yr)	(PTE)	Units	(lbs/hr)	(tons/yr)	Determination
Pollutants:							
1.)	See Attached						
2.)							
3.)							
4.)							
5.)							
6.)							
7.)							
8.)							

Greenhouse Gases (GHGs)

		Effic	ciency Standards	7		
	Pre-Controlled	Potential		Potential	Potential	
	Potential Emissions	to Emit		to Emit	to Emit	Basis for
	(tons/yr)	(PTE)	Units	(lbs/hr)	(tons/yr)	Determination
Pollutants:	<u> </u>					
1.)						
2.)						
3.)						
4.)						
5.)						
6.)						
7.)						
8.)						

Separator/Treater

Company Equipment ID:	Roger Leo Fe	ederal Heater Treater
Company Equipment Description:	-1	Heater Treater
blow a lower press, the		
Operating Status: Operating		
Initial Construction Commenceme		Oct 2014 - Feb 2015
Initial Operation Commencement		4/2/2015
Most Recent Construction/ Modifi	cation	
Commencement Date:		NA
Most Recent Operation Commence	ement Date:	NA
8		ncluded in this application (must be completed regardless of date
of installation or modification):		
Reason: Construction	n (Greenfield	d/New Facility)
Type of Vessel: Heater	-Treater 80-145	Is Vessel Heated? Yes
The second of th	25-75	
SCC Codes: List all Source Classifications source (e.g., 1-02-002-04).	ation Code(s)	(SCC) that describe the process(es) performed by the emission 31000129
Potential Operating Schedule:	Provide the	operating schedule for this emission unit.
1999 14 9	24	
	8760	

Control Equipment: Yes	
If yes, please fill out and attach the appropriate Control Device and Release Point Information	ion worksheets.
Best Available Control Technology (BACT): Was a BACT Analysis completed for this emission	unit?
Yes No X	
Pollutant:	
Proposed BACT: Presumptive BACT- Smokeless Combustor 98% control, but all gas is ty	pically sold
*If yes, attach BACT Analysis with this application.	
Lowest Achievable Emission Rate (LAER): Was a LAER Analysis completed for this emission u	ınit?
Yes No X	
Pollutant:	
Proposed LAER:	
*If yes, attach LAER Analysis with this application.	
Federal and State Rule Applicability:	
New Source Performance Standards (NSPS): Not Affected	
New Source Performance Standard are listed under 40 CFR 60-	
Standards of Performance for New Stationary Sources.	
NSPS Subpart:	
ALL DESCRIPTION OF THE PROPERTY OF THE PROPERT	Nat Affactad
National Emission Standards for Hazardous Air Pollutants (NESHAP Part 61):	Not Affected
National Emissions Standards for Hazardous Air Pollutants (NESHAP Part 61) are	listed under 40 CFR
61. (These include asbestos, benzene, beryllium, mercury, and vinyl chloride).	
Part 61 NESHAP Subpart:	
National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63):	Not Affected
National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63)	
standards are listed under 40 CFR 63	
Part 63 NESHAP Subpart:	
Prevention of Significant Deterioration (PSD): Not Affected]
These rules are found under WAQSR Chapter 6, Section 4.	-
Non-Attainment New Source Review: Not Affected	
These rules are found under WAQSR Chapter 6, Section 13.	

Storage Tank/Silo

Company Equipment ID:	Roger Leo Fe	ederal Crude Oil Tank	s 1-8		
Company Equipment Description		Crude Tanks 1-8			
	<u> </u>				To the second of the
Operating Status: Operating		51	or to river a state	THE WATER	
Initial Construction Commencem			14 - Feb 2015		
Initial Operation Commencement			Apr-15	Mail dogs	Trin desectors a mucol
Most Recent Construction/ Modi	fication				
Commencement Date:		·	NA		and the problem
Most Recent Operation Commen	cement Date:		NA		
Select reason(s) for this emission		naludad in this annlis		ha samulat	
installation or modification):	is unit being i	nciuded in this applic	cation (must	be complet	ted regardless of date of
Reason: Construction	on (Greenfield	d/New Facility)	-/20/50/1-1		
Reason. Constructi	on (oreenned	a/New racinty)			
If reason is <i>Reconstruction</i> or <i>Tell</i> Material Type: Liquid	mporary Perm		Les millions		and the first of t
Description of Material Stored:		Crude Oil from Oil w	ell productio	n	
Capacity: 400		Units:	lh a uu a la	1	<u> CALESTO</u>
Maximum Throughput:	513.92	- 01111.5.	barrels	_ Units:	harrole/day
Maximum Hourly Throughput:	42.83	State of the state of	<u>Lai</u> r en verns	Units:	barrels/day barrels/hr
Operating Pressure (psig):	Atmosphere			Offics.	Darreis/III
Vapor Pressure of Material Store		RVP 5.4			
Is Tank Heated?: No		-			
SCC Codes: List all Source Classific source (e.g., 1-02-002-04).	cation Code(s)	(SCC) that describe t	he process(e	s) performe	ed by the emission
		2310010200			14 Art 1/5 Ported to 18co
Potential Operating Schedule: Hours/day:	Provide the o	operating schedule fo	or this emission	on unit.	
Hours/year:	8760				

Control Equipment: Yes If yes, please fill out and attach the appropriate Control Device and Release Point Information (Control Device).	rmation worksheets.
Best Available Control Techology (BACT): Was a BACT Anal s completed for this emi	ission unit?
Yes No	
Pollutant:	
Proposed BACT: Presumptive BACT- Smokeless Combustor 98% control	
*If yes, attach BACT Analysis with this application.	
Lowest Achievable Emission Rate (LAER): Was a LAER Analyst completed for this emiss	sion unit?
Tes .	
Pollutant:Proposed LAER:	
*If yes, attach LAER Analysis with this application.	
ii yes, accaen exercitarysis wen eins approacioni	
Federal and State Rule Applicability: New Source Performance Standards (NSPS): New Source Performance Standard are listed under 40 CFR 60- Standards of Performance for New Stationary Sources. NSPS Subpart:	
National Emission Standards for Hazardous Air Pollutants (NESHAP Part 61):	Not Affected
National Emissions Standards for Hazardous Air Pollutants (NESHAP Part 61 61. (These include asbestos, benzene, beryllium, mercury, and vinyl chloride) Part 61 NESHAP Subpart:	
National Engineers Chandands for Hannadays Air Pollytonts (NECHAR Port 62)	Not Affected
National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63): National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63) standards are listed under 40 CFR 63 Part 63 NESHAP Subpart:	
Prevention of Significant Deterioration (PSD): Not Affected These rules are found under WAQSR Chapter 6, Section 4.	
Non-Attainment New Source Review: Not Affected These rules are found under WAQSR Chapter 6, Section 13.	

Storage Tank/Silo

Company Equipment ID:	Roger Leo Fe	ederal Produced Wat	er Tanks		
Company Equipment Description	1:	Produced Water 1,	Produced Wa	ater 2	
Operating Status: Operating					
Initial Construction Commencem		Oct 20)14 - Feb 201	5	
Initial Operation Commencemen	t Date:	11-1-11-11-11-11-11-11-11-11-11-11-11-1	Apr-15	12111111	Minar Mare in three was
Most Recent Construction/ Mod	ification	66			[m]
Commencement Date:			NA		
Most Recent Operation Commer	ncement Date:		NA		
Select reason(s) for this emissio installation or modification):	ns unit being i	included in this appl	ication (must	be comple	eted regardless of date of
Reason: Construct	ion (Greenfiel	d/New Facility)	- Telephone		
	ion (oreenine)	dy recti r demey)			
Material Type: Liquid Description of Material Stored:		Produced water fro		oduction	
Capacity: 400		Units:	barrels		
Maximum Throughput:	718		<u> </u>	Units:	barrels/day
Maximum Hourly Throughput:	59.83			Units:	barrels/hr
Operating Pressure (psig):	Atmosphere		1 10		
Vapor Pressure of Material Store	d (psig):	1 (water)		<u></u>	
Is Tank Heated?: No					
SCC Codes: List all Source Classifi source (e.g., 1-02-002-04).	cation Code(s)) (SCC) that describe 2310010200	the process(e	es) perform	ned by the emission
Potential Operating Schedule:	Provide the	operating schedule f	or this emissi	ion unit.	
Hours/day:	24				
Hours/year:	8760				

Control Equipment: If yes, please fill out a	Yes and attach the appropriat	e Control Devi	ice and Release Po	int Informatio	on worksheets.
Best Available Contro	l Technology (BACT): Wa	s a BACT Ar	ysis completed for	this emission	unit?
Yes	0 , (,	No			
Pollutant:					
Proposed BACT:					
*If yes, attach BACT A	nalysis with this application	on.			
Lowest Achievable En	nission Rate (LAER): Was	a LAER Analys	s completed for th	is emission u	nit?
Pollutant:		NO			
Proposed LAER:					
	nalysis with this applicatio	n.			
Federal and State Rul		_			
	e Performance Standard o of Performance for New S	are listed unde			
National Emission Star	ndards for Hazardous Air F	Pollutants (NES	SHAP Part 61):		Not Affected
National E. 61. (These	missions Standards for Ha include asbestos, benzer SHAP Subpart:	azardous Air P	ollutants (NESHAF		listed under 40 CFR
National Emission Star	ndards for Hazardous Air F	Pollutants (NES	SHAP Part 63):		Not Affected
National E standards	mission Standards for Haz are listed under 40 CFR 6 SHAP Subpart:	zardous Air Po		Part 63)	
	nt Deterioration (PSD): s are found under WAQSF		ot Affected Section 4.		
Non-Attainment New <i>These rule</i>	Source Review: s are found under WAQSF	Not Affected R Chapter 6, S	Section 13.		

Control Equipment:

Flare/Combustor

Manufacturer:	Steffes			Date Installed:		Oct 2014 - Fel	b 2015
Model Name and				Company Contro	I		
Number:	Dual Tip (low and high	pressure)		Equipment ID:			
Company Control Equ						Roger Leo Fed	deral Flare
Description:	Roger Leo F	ederal tank v	apor and	emergency gas fla	re		
			•	<u> </u>			
Pollutant(s) Controlle	ed: CO	NOx	Pb	SO2	VOC	PM	
PM (FIL)	PM Condensable	PM 10	(FIL)	PM 2.5 (FIL	.)	PM 10	PM 2.5
Other HAPs		•					
				_			
NOTE: The following	g fields require numeric v	alues unless	otherwise	denoted with an	asteris	k*	
Maximum Design Cap	pacity (MMSCF/hr):	High pressur	e tip 1.1, l	ow 0.006 MMscf/	hr		
Minimum Design Cap	pacity (MMSCF/hr):			11, low 4.4 scf/hr			
Design Control Efficie				ficiency (%):			
Operating Control Eff	ficiency (%):	98	•	, , ,		123.11	
Flare Type:*	Elevated- Open	E	levated F	lare Type:*	Non-A	ssisted	
Ignition Device:*	Yes	Fla	me Prese	ence Sensor:* Yes		900	
Inlet Gas Temp (F):	ambient at 90F			Flame Presence	Type:*	Othe	er
Gas Flow Rate (acfm)	: va	ries		Outlet Gas Temp		900	
This is the	e only control equipment	on this air co	ntankani	to be a series of the property			
If not, this control eq		Prima		Secondary		Paral	lel
P. C. H. Alexander							
List all other emissio							
vented to this contro	ol equipment:*	This Flare	controls	tank vapors, and	associat	ted gas in eme	rgency
List all release point	IDs associated with this	situations w	hen it can	not be sold (or co	nsume	d by the treate	er heater).
control equipment:*		Tanks & Hea	ter Treate	er (in emergencies)		

Emissions Information- The following tables request information needed to determine the applicable

requirements and the compliance status of this emission unit with those requirements.

Efficiency Standards

			iency Standards			
	Pre-Controlled	Potential		Potential	Potential	
	Potential Emissions	to Emit		to Emit	to Emit	Basis for
	(tons/yr)	(PTE)	Units	(lbs/hr)	(tons/yr)	Determination
Criteria Pollutants:				•	•	
1.)						
Particulate emissions						
(PE/PM) (formerly						
particulate matter,						
PM)						
2.)						
PM #10 microns in	1					
diameter (PE/PM10)						
3.)						
PM #2.5 microns in						
diameter (PE/PM2.5)						
4.) Sulfur dioxide (SO2)						
5.) Nitrogen Oxides		0.14	lb/MMBtu	1.12	4.894765	AP-42
(NOx)		0.14	ID/IVIIVIBLU	1.12	4.034703	A1 - 42
6.) Carbon monoxide		0.37	lb/MMBtu	2.95	12.93616	AP-42
(CO)		0.57	ID/IVIIVIDEA	2.55	12.55010	711 12
7.) Volatile organic	1436.37			6.56	28,7274	Tanks Program
compounds (VOC)	1450.57			0.50	2017271	7411167116814111
8.) Lead (Pb)						
9.) Total Hazardous Air	42.97			0.20	0.8594	Tanks Program
Pollutants (HAPs)	42.57			0.20	0.000	74,116,116,111
10.) Fluoride (F)				3		
11.) Hydrogen Sulfide						
(H2S)						
12.) Mercury (Hg)						
13.) Total Reduced Sulfur						
(TRS)						
14.) Sulfuric Acid Mist						
(SAM)		. , "				

^{*}Provide your calculations as an attachment and explain how all process variables and emissions factors were selected.

Hazardous Air Pollutants (HAPs) and Toxic Air Contaminants

			Effici	ency Standards			
		Pre-Controlled Potential Emissions (tons/yr)	Potential to Emit (PTE)	Units	Potential to Emit (lbs/hr)	Potential to Emit (tons/yr)	Basis for Determination
utants	:				•		
1.)	See Attached						
2.)		5,11,75,0 -1 15 1					
3.)							
4.)							
5.)						F-11-11-11-11	THE THE SET TO
6.)		PA PA					I forum street
7.)							
8.)							

Greenhouse Gases (GHGs)

		Efficier	icy Standards	a the state of the	Url bal inch	
	Pre-Controlled Potential Emissions (tons/yr)	Potential to Emit (PTE)	Units	Potential to Emit (lbs/hr)	Potential to Emit (tons/yr)	Basis for Determination
Pollutants:						
1.)						
2.)						
3.)						
4.)						
5.)						
6.)						MESTER STATE
7.)						
8.)						

Fugitives

Company Equipment ID:	Roger Leo Fe	deral Fugs		
Company Equipment Description:		Fugitive Em	ssions	
Operating Status: Operating				
Initial Construction Commenceme	ent Date:		Oct 2014 - Feb 2015	
Initial Operation Commencement	Date:		Apr-15	
Most Recent Construction/ Modif	ication			
Commencement Date:			NA	
				
Most Recent Operation Commend	cement Date:		NA	
Select reason(s) for this emission	s unit being in	cluded in thi	s application (must be comp	leted regardless of date of
installation or modification):				
Reason: Constructi	on (Greenfield	I/New Facility)	
If reason is <i>Reconstruction</i> or <i>Ter</i>	nporary Perm	it or Other,	olease explain below:	
Type of Fugitive Emission:	Fugitive Leak	s at O&G		
		(<u>)</u>		11 11
SCC Codes: List all Source Classific	ation Code(s)	(SCC) that de	scribe the process(es) perfori	med by the emission source
(e.g., 1-02-002-04).				
		310888	311	
Potential Operating Schedule:		pperating sch	edule for this emission unit.	
Hours/day:	24			
Hours/year:	8760			

Control Equipment: No	efficiency of the second of the second
If yes, please fill out and attach the appropriate Control Device and Release Point Informat	ion worksheets.
Best Available Control Technology (BACT): Was a BACT Analysis completed for this emission	n unit?
Yes No	
Pollutant:	parente Kultur
Proposed BACT:	
*If yes, attach BACT Analysis with this application.	
Lawret Ashiovable Emission Pate (LAER) Was LAER A. L	1.2
Lowest Achievable Emission Rate (LAER): Was a LAER Analysis completed for this emission	unit?
Yes No	
Pollutant:Proposed LAER:	
*If yes, attach LAER Analysis with this application.	
if yes, attach LAER Analysis with this application.	
Federal and State Rule Applicability:	
New Source Performance Standards (NSPS): Not Affected	
New Source Performance Standards (NSFS). New Source Performance Standard are listed under 40 CFR 60-	
Standards of Performance for New Stationary Sources.	
NSPS Subpart:	
National Emission Standards for Hazardous Air Pollutants (NESHAP Part 61):	Not Affected
National Emissions Standards for Hazardous Air Pollutants (NESHAP Part 61) are	listed under 40 CFR 61.
(These include asbestos, benzene, beryllium, mercury, and vinyl chloride).	
Part 61 NESHAP Subpart:	
National Emission Charles I. C. H. A. C	
National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63):	Not Affected
National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63)	
standards are listed under 40 CFR 63	
Part 63 NESHAP Subpart:	
Prevention of Significant Deterioration (PSD): Not Affected	The Control of March
These rules are found under WAQSR Chapter 6, Section 4.	_
Non-Attainment New Source Review: Not Affected	
These rules are found under WAQSR Chapter 6, Section 13.	

Emissions Information- The following tables request information needed to determine the applicable

requirements and the compliance status of this emission unit with those requirements.

Efficiency Standards

				ciency Standards			
		Pre-Controlled	Potentiai		Potential	Potentiai	
		Potential Emissions	to Emit		to Emit	to Emit	Basis for
		(tons/yr)	(PTE)	Units	(lbs/hr)	(tons/yr)	Determination
Criteria Po	llutants						
						1	
1.)							
	Particulate emissions						
	(PE/PM) (formerly						
	particulate matter,						
	PM)						
2.)							
1	PM #10 microns in						
	diameter (PE/PM10)						
3.)							
] 3.,	PM #2.5 microns in						
	To state the state of the state						
	diameter (PE/PM2.5)					-	
	Sulfur dioxide (SO2)						
5.)	Nitrogen Oxides						
	(NOx)						
6.)	Carbon monoxide						
	(CO)						
7.)	Volatile organic				1.00	4.36	Other
1	compounds (VOC)				1.00	4.50	Other
8.1	Lead (Pb)						
	Total Hazardous Air				29 100015	1501 10000	
] 3.,	Pollutants (HAPs)				0.15	0.66	Other
10.)	Fluoride (F)						
11.)	Hydrogen Sulfide						
	(H2S)						
	Mercury (Hg)						
13.)	Total Reduced Sulfur						
	(TRS)						N. C.
14.)	Sulfuric Acid Mist						
	(SAM)						
	1//						1

^{*}Provide your calculations as an attachment and explain how all process variables and emissions factors were selected.

Hazardous Air Pollutants (HAPs) and Toxic Air Contaminants

			Effici	ency Standards			
		Pre-Controlled Potential Emissions (tons/yr)	Potential to Emit (PTE)	Units	Potential to Emit (lbs/hr)	Potential to Emit (tons/yr)	Basis for Determination
ollutants							
1.)	NA						
2.)							
3.)							
4.)							
5.)					1000		11112 1111112971 12171
6.)						100	Hebrer Hebrer
7.)							
8.)							

Greenhouse Gases (GHGs)

		Efficiency Standards		al labbay		
	Pre-Controlled	Potential		Potential	Potential	T
	Potential Emissions	to Emit	15 o 3 o 000 o 6	to Emit	to Emit	Basis for
	(tons/yr)	(PTE)	Units	(lbs/hr)	(tons/yr)	Determination
Pollutants:				-		
1.) NA					T	
2.)						1. 9.11 1.7.1
3.)						
4.)						
5.)						
6.)				111		y all the state of the
7.)						LYNOT HI HIS
8.)			the transfer of the state of	100		et in mert hallen

Loading/Unloading/Dump

Company Equipment ID:	Roger Leo Fed	deral Truck Loading		
Company Equipment Description:		Loading		
Operating Status: Operating				
Initial Construction Commenceme	ent Date:	Oct 2014	- Feb 2015	_
Initial Operation Commencement	Date:	Apr	r-15	_
Most Recent Construction/ Modif	ication			
Commencement Date:		N	IA	_
Most Recent Operation Commenc	cement Date:	N	IA	
Select reason(s) for this emission	s unit being inc	cluded in this application	on (must be complete	d regardless of date of
installation or modification):				
Reason: Construction	on (Greenfield/	New Facility)		
If reason is Reconstruction or Ten	nporary Permit	t or Other, please expla	ain below:	
Type of Material: Liquid	1			
Material Description:	Crude Oil and	Produced Water		
Maximum Annual Throughput:	95300		Units:	barrels/yr
Maximum Hourly Throughput:	85		Units:	barrels/hr
Detailed Description of Loading/U	nloading/Dum	p Source:		
Crude Oil and Produced water fro	m oil well	9		
	-			
SCC Codes: List all Source Classific	ation Code(s) (SCC) that describe the p	process(es) performed	by the emission source
(e.g., 1-02-002-04).	() (, ,,	i.
(c.g.) 1 01 001 0 1).				
		2310010800		
		2310010000		
Potential Operating Schedule:	Provide the or	perating schedule for th	is emission unit.	
Hours/day:	4			
Hours/year:	1460			
110013/ 4001.				

Control Equipment: No	sto Control Do	sian and Balanca B	-int Info	n - min min min i promi
If yes, please fill out and attach the appropriate	te Control Dev	nce and kelease P	oint informatio	n worksneets.
Best Available Control Technology (BACT): Wa	as a BACT Ana	lysis completed for	r this amission i	ınit?
Yes	No No	rysis completed to	tills cillission (anne:
Pollutant:				
Proposed BACT:				
*If yes, attach BACT Analysis with this application	on.			to his office to the
		~		
Lowest Achievable Emission Rate (LAER): Was	s a LAER Analy	sis completed for t	his emission ur	nit?
Yes	No			
Pollutant:				
Proposed LAER:			19.1	rank i msaj
*If yes, attach LAER Analysis with this application	on.			
Fadaval and China D. L. A. H. 1919				
Federal and State Rule Applicability:	1			
New Source Performance Standards (NSPS):	L	Not Affected		
New Source Performance Standard				
Standards of Performance for New S NSPS Subpart:	Stationary Sou	irces.		
Noi 3 Subpart.				
National Emission Standards for Hazardous Air	Pollutants (NE	SHAP Part 61):		Not Affected
National Emissions Standards for Ha				isted under 40 CFR 61.
(These include asbestos, benzene, l	beryllium, mer	cury, and vinyl chlo	oride).	
Part 61 NESHAP Subpart:				T probably at
National Emission Standards for Hazardous Air	Pollutants (NF	SHAP Part 63):		Not Affected
National Emission Standards for Ha			Part 63)	TVOT / III COLCU
standards are listed under 40 CFR 6		onatanto (NEOTI)	, art 60)	
Part 63 NESHAP Subpart:				
Prevention of Significant Deterioration (PSD):	n lander to the	Not Affected		1
These rules are found under WAQS.	L			_
ss .a.s a.s .sa.ra andor wings	Shaptor 0, t	000.017 1.		
Non-Attainment New Source Review:	Not Affecte	d		
These rules are found under WAQS	R Chapter 6,	Section 13.		

Emissions Information- The following tables request information needed to determine the applicable

requirements and the compliance status of this emission unit with those requirements.

			Efficiency Standards				
		Pre-Controlled	Potential		Potential	Potential	
		Potential Emissions	to Emit		to Emit	to Emit	Basis for
		(tons/yr)	(PTE)	Units	(lbs/hr)	(tons/yr)	Determination
Criteria Po	llutants:						
1.)							
	Particulate emissions	at the state of th					
	(PE/PM) (formerly						
	particulate matter,						
	PM)						
2.)							
	PM #10 microns in						
	diameter (PE/PM10)						
3.)							
'	PM #2.5 microns in						
	diameter (PE/PM2.5)						
4.)	Sulfur dioxide (SO2)						
	Nitrogen Oxides						
'	(NOx)						
6.)	Carbon monoxide						
	(CO)						
7.)	Volatile organic		1.366**		7.37	5.38	AP-42
	compounds (VOC)		1.500		7.57	3.30	711 12
8.)	Lead (Pb)						
9.)	Total Hazardous Air				1.11	0.81	AP-42
	Pollutants (HAPs)				1.11	0.01	711 12
10.)	Fluoride (F)						
11.)	Hydrogen Sulfide						
	(H2S)						
12.)	Mercury (Hg)						
13.)	Total Reduced Sulfur						
	(TRS)						
14.)	Sulfuric Acid Mist						
	(SAM)						

^{*}Provide your calculations as an attachment and explain how all process variables and emissions factors were selected.

^{**} lb/1000 gallons, uncontrolled PTE based on operating 8760 hours

Hazardous Air Pollutants (HAPs) and Toxic Air Contaminants

Efficiency Standards

			LITIC	iericy Staridards			
		Pre-Controlled	Potential		Potential	Potential	
		Potential Emissions	to Emit		to Emit	to Emit	Basis for
		(tons/yr)	(PTE)	Units	(lbs/hr)	(tons/yr)	Determination
ollutants:							
1.)	NA	The state of the s		Tarrela 2 Coch			
2.)							
3.)		1 1199911				All trust	
4.)	7/ 1/	3.39	1,519 (2.17)	M SEE TO BE READ.	2 111 30 9 3	TO DO TO	ELVILLE BERTON
5.)	DINGS	1 Edit - Sa		19 colai 11			
6.)		ates	Trail mou	KAN WENT	21,000,000		
7.)							
8.)							
			Effic	iency Standards	7		
		Pre-Controlled Potential Emissions (tons/yr)	Potential to Emit (PTE)	Units	Potential to Emit (lbs/hr)	Potential to Emit (tons/yr)	Basis for Determination
ollutants:							
	NA	3177	Tell III	BYELL EASI			BUT SETTINGK
2.)		f (§		post in al			
3.)			La di La nida	nedlskuddl			
4.)			1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1	Alabama Nama II			
5.)							
6.)							
7.)				12372 [18]			
8)			1 10/10/10 10/10	NO COURTE		79-	

Release Point Information:

Complete the table below for *each* release point. Please include release point information for each emission unit. Multiple attachments may be necessary. A release point is a point at which emissions from an emission unit are released into the ambient (outside)air. List each individual release point on a separate pair of lines (release point ID and description). For longitude and latitude, use NAD 83/WGS84 datum and 5 digits after the decimal (i.e. 41.12345, -107.56789)

Stad	ck Release Point Inform	ation	
Company Release Point ID:	Release Point Type:	Vertical	
Controlled Tank & Emergency gas Emissions	Release Point Latitude	:	43.25716
30.000	Release Point Longitud	de:	-105.789419
Company Release Point Description:	Base Elevation (ft):	5576	
Tank vapor and Associated gas combustor	Stack Height (ft):	20	
emissions	Stack Diameter (ft):	0.25	
	Exit Gas Velocity (ft/s)	:	300
	Exit Gas Temp (F):	900	
	Exit Gas Flow Rate (ac	fm):	1178
Company Release Point ID:	Release Point Type:	Vertical	
Heater Treater heater	Release Point Latitude	2:	43.25716
	Release Point Longitud	de:	-105.789419
Company Release Point Description:	Base Elevation (ft):	5198	
	Stack Height (ft):	20	
	Stack Diameter (ft):	1	
	Exit Gas Velocity (ft/s)	:	7.2
	Exit Gas Temp (F):	575	
	Exit Gas Flow Rate (ac	fm):	340
Company Release Point ID:	Release Point Type:		
	Release Point Latitude		
	Release Point Longitud	de:	
Company Release Point Description:	Base Elevation (ft):	(()	
	Stack Height (ft):		
	Stack Diameter (ft):		
	Exit Gas Velocity (ft/s)	:	
	Exit Gas Temp (F):		
	Exit Gas Flow Rate (ac	fm):	
Company Release Point ID:	Release Point Type:		
	Release Point Latitude	:	
	Release Point Longitud	de:	
Company Release Point Description:	Base Elevation (ft):	(New york and a second	
	Stack Height (ft):		
	Stack Diameter (ft):		
	Exit Gas Velocity (ft/s)	:	
	Exit Gas Temp (F):		
	Exit Gas Flow Rate (ac	fm):	

Complete the table below for each fugitive (area, volume, line) release point. List each individual release point on a separate line.

Fugitive Release Point Information							
Company Release Point ID:	Release Point Latitude:	43.25716					
Fugs	Release Point Longitude:	-105.88214					
	Release Height (ft): between	en 1 and 30					
Company Release Point Description:							
Fugitives, which by definition do not have a							
point, volume or line							
Company Release Point ID:	Release Point Latitude:						
	Release Point Longitude:						
	Release Height (ft):						
Company Release Point Description:							
Company Release Point ID:	Release Point Latitude:						
	Release Point Longitude:						
	Release Height (ft):						
Company Release Point Description:							
Company Release Point ID:	Release Point Latitude:						
	Release Point Longitude:						
	Release Height (ft):						
Company Release Point Description:							

			ji.	

SM ENERGY Roger Leo Federal COMBUSTION EMISSIONS

Compound	Emission Factor (lb/10 ⁶ ft ³)	Emission Factor (lb/MMBtu)	Treaters - 0.75 MMBtu/hr PTE (TPY)	Emission Factor Source
CO	84	0.082352941	0.271	AP-42 Table 1.4-1
NO _x	100	0.098039216	0.322	AP-42 Table 1.4-1
SO ₂	0.6	0.000588235	0.002	AP-42 Table 1.4-2
VOC	5.5	0.005392157	0.018	AP-42 Table 1.4-2
Total HAPs	-		0.006	
2-Methylnaphthalene	2.4E-05	2.4E-08	7.7E-08	AP-42 Table 1.4-3
3-Methylchloranthrene	1.8E-06	1.8E-09	5.8E-09	AP-42 Table 1.4-3
7,12-Dimethylbenz(a)anthracene	1.6E-05	1.6E-08	5.2E-08	AP-42 Table 1.4-3
Acenaphthene	1.8E-06	1.8E-09	5.8E-09	AP-42 Table 1.4-3
Acenaphthlyene	1.8E-06	1.8E-09	5.8E-09	AP-42 Table 1.4-3
Anthracene	2.4E-06	2.4E-09	7.7E-09	AP-42 Table 1.4-3
Benz(a)anthracene	1.8E-06	1.8E-09	5.8E-09	AP-42 Table 1.4-3
Benzene	2.1E-03	2.1E-06	6.8E-06	AP-42 Table 1.4-3
Benzo(a)pyrene	1.2E-06	1.2E-09	3.9E-09	AP-42 Table 1.4-3
Benzo(b)fluoranthene	1.8E-06	1.8E-09	5.8E-09	AP-42 Table 1.4-3
Benzo(g,h,i)perylene	1.2E-06	1.2E-09	3.9E-09	AP-42 Table 1.4-3
Benzo(k)fluoranthene	1.8E-06	1.8E-09	5.8E-09	AP-42 Table 1.4-3
Chrysene	1.8E-06	1.8E-09	5.8E-09	AP-42 Table 1.4-3
Dibenzo(a,h)anthracene	1.2E-06	1.2E-09	3.9E-09	AP-42 Table 1.4-3
Dichlorobenzene	1.2E-03	1.2E-06	3.9E-06	AP-42 Table 1.4-3
Fluoranthene	3.0E-06	2.9E-09	9.7E-09	AP-42 Table 1.4-3
Fluorene	2.8E-06	2.7E-09	9.0E-09	AP-42 Table 1.4-3
Formaldehyde	7.5E-02	7.4E-05	2.4E-04	AP-42 Table 1.4-3
Hexane	1.8E+00	1.8E-03	5.8E-03	AP-42 Table 1.4-3
Indeno(1,2,3-cd)pyrene	1.8E-06	1.8E-09	5.8E-09	AP-42 Table 1.4-3
Naphthalene	6.1E-04	6.0E-07	2.0E-06	AP-42 Table 1.4-3
Phenanthrene	1.7E-05	1.7E-08	5.5E-08	AP-42 Table 1.4-3
Pyrene	5.0E-06	4.9E-09	1.6E-08	AP-42 Table 1.4-3
Toluene	3.4E-03	3.3E-06	1.1E-05	AP-42 Table 1.4-3
Arsenic	2.0E-04	2.0E-07	6.4E-07	AP-42 Table 1.4-4
Beryllium	1.2E-05	1.2E-08	3.9E-08	AP-42 Table 1.4-4
Cadmium	1.1E-03	1.1E-06	3.5E-06	AP-42 Table 1.4-4
Chromium	1.4E-03	1.4E-06	4.5E-06	AP-42 Table 1.4-4
Cobalt	8.4E-05	8.2E-08	2.7E-07	AP-42 Table 1.4-4
Manganese	3.8E-04	3.7E-07	1.2E-06	AP-42 Table 1.4-4
Mercury	2.6E-04	2.5E-07	8.4E-07	AP-42 Table 1.4-4
Nickel	2.1E-03	2.1E-06	6.8E-06	AP-42 Table 1.4-4
Selenium	2.4E-05	2.4E-08	7.7E-08	AP-42 Table 1.4-4

SM ENERGY Roger Leo Federal

CONTROLLED TANK EMISSIONS CO and NOx Emissions From Combustion of Tank Vapors

Compound	Emission Factor (lb/MMBtu)	Throughput MMBtu/yr	Controlled Emissions (TPY)	Emission Factor Source
CO	0.37	69,925	12.936	AP-42 Table 13.5-1
10 _x	0.14	69,925	4.895	AP-42 Table 13.5-1

HC Vapor emissions (MSCFD) =

70.4800

Gas Heat Content (Btu/SCF) =

2,718.16

Annual heat throughput (Btu/yr) =

69,925,209,632

^{*} Both the throughput and heat content are from the E&P TANKS results - attached.

VOC and HAPs Emissions From Combustion of Tank Vapors							
Compound Throughput Burner Control Controlled Emissions Emission Factor Sou							
VOC	1436.37	98	28.727	WY Oil and Gas Guidance -2010			
HAPs	42.97	98	0.859	WY Oil and Gas Guidance -2010			

Emissions are based on 98% control efficiency.

Production values put in E&P TANKS is incorporating a decline curve of 0.6 to account for the decrease in production during the first year

Roger Leo Federal **SM ENERGY**

FUGITIVE EMISSIONS

				Emissions		
Total Component Count	nent Count	Hydrocarbon EF (lb/component-day)	ТРУ НС	HC VOC Wt. Fraction	TPY VOCs	
Valves	84	0.13	1.99	1	1.99	66
Flanges	84	0.0058	60.0	1	0.09	60
Connectors	238	0.011	0.48	1	0.48	48
Open-ended lines	20	0.074	0.27	1	0.27	27
Other components	21	0.4	1.53	1	1.53	53
Total	447		4.36		4.36	36

Total HCs =	4.36 TPY
l otal VOC's = Fotal VOC's =	4.36 IPY 1.00 lb/hr
Fotal HAPs =	0.66 TPY
Fotal HAPs =	0.15 lb/hr

- Component counts were derived from Table W-1C of Subpart W (Oil and Natural Gas Systems) of 40 CFR
- Part 98 for Western U.S. oil production equipment for wellheads and heater treater. Tank components are based on engineering estimates. - Emission Factors (in Ib/component-day) from Wyoming Air Quality Division Oil and Gas Permitting Guidance, 2007
 - Light Oil VOC Weight fraction assumed to be 1.0 to be conservative
- · To be conservative, all Speciated Fugitive Emission Factors (Wt Fractions) from light crude Wyoming Air Quality Division Oil and Gas Permitting Guidance, 2007 (HAP Fraction of Hydrocarbon Emissions 0.2585)
 - Total HAPs calculated by multiplying Total HCs in TPY by weight fraction HAPs

		*	ė.

SM ENERGY Roger Leo Federal LOADING EMISSIONS

Truck Loading Emission Methodology

 L_L = 12.46 x $\frac{SPM}{T}$

Where:

 $L_L = loading loss (lb/1,000 gallon liquid loaded)$

S = saturation factor (AP-42 Table 5.2-1)

P = true vapor pressure of liquid loaded (psia), (from AP-42 Table 7.1-2)

M = molecular weight of vapor (Table 7.1-2) T = Temperature of liquid loaded (${}^{\circ}R = 460 + {}^{\circ}F$)

Variables		Source
S	0.6	AP-42 Table 5.2-1 (Submerged loading: dedicated normal service)
P (psia)	1.9	AP-42 Table 7.1-2 (Crude Oil RVP 5 at 40F)
M (lb/lbmole)	50	AP-42 Table 7.1-2 (Crude Oil RVP 5)
T (°R)	520	Annual average temperature (60°F)
L _L (lb/1,000 gal)	1.366	=
		Total production from well (including a decline factor of 40% to account for the decrease in
Loading (bbl/day)	513.9	production during the first year)
Loading (bbl/yr)	187,574	
HAP Fraction (wt.)	0.15	Low Pressure Oil Sample

		Truck Load	ding	Emission Estir	mates	3		
VOC (TPY)	=	Annual Production (bbl)	х	42 (gal) bbl	х -	1 1000	х —	L _L (lb) 1,000 gallon
			Х	1 (ton) 2,000 (lb)	=	5.38		Ton VOC/yr
VOC (lb/hr)	=	VOC (ton)	х	2,000 (lb) 1 (ton)	x ·	1 yr 1,460 hrs		
				18	=	7.37		lb VOC/hr
HAP (TPY)	=	VOC (ton) yr	х	HAP Fraction	=1	0.81		Ton HAP/yr
HAP (lb/hr)	=	VOC (lb)	х	HAP Fraction	=	1.11		lb HAP/hr

		J	u
			4

```
RMR-S Snake Charmer Draw Roger Leo Fed 3875-20-29-1FH 20150520 EP Tanks.txt
*************************
    Project Setup Information
*************************
Project File
\\tsclient\M\StoV\SMEnergy-Air\ProjectDocuments\AirPermitCompliance\Wyoming\PowderRi
verBasin\Permits\RogerLeoFed 3875\Roger Leo Fed E&P Tanks.ept
Flowsheet Selection : Oil Tank with Separator
Calculation Method
                     : RVP Distillation
Control Efficiency
                     : 98.0%
Known Separator Stream : Low Pressure Oil
Entering Air Composition : No
Filed Name
                      : Roger Leo Fed (Allemand sample)
Well Name
                      : SM Energy
                      : 2015.05.18
Date
*************************
    Data Input
*************************
****
Separator Pressure : 28.00[psig]
Separator Temperature : 66.00[F]
Ambient Pressure
                     : 12.00[psia]
Ambient Temperature
                    : 60.00[F]
C10+ SG
                    : 0.7409
C10+MW
                      : 152.16
-- Low Pressure Oil
  No.
        Component
                           mo1 %
                           0.0000
  1
        H2S
  2
        02
                         0.0000
  3
        CO2
                          0.0453
  4
                          0.0000
        N2
  5
        C1
                           0.7862
  6
        C2
                         1.9621
  7
        C3
                           5.1680
  8
        i-C4
                          1.4954
  9
        n-C4
                          5.3805
  10
        i-C5
                           3.7862
  11
        n-c5
                           4.5463
  12
        C6
                           5.8584
                          22.1463
  13
        C7
  14
        C8
                           9.6358
  15
        C9
                           7.2007
  16
        C10 +
                          16.2578
  17
        Benzene
                           0.8710
  18
        Toluene
                           3.7437
  19
        E-Benzene
                           0.3641
                           4.3996
  20
        Xylenes
  21
        n-c6
                           5.2991
  22
        224Trimethylp
                           1.0535
-- Sales Oil
```

RMR-S Snake Charmer Draw Roger Leo Fed 3875-20-29-1FH 20150520 EP Tanks.txt

: 513.6[bb]/day] : 365 [days/year] : 43.9 Production Rate Days of Annual Operation

API Gravity

Reid Vapor Pressure : 5.40[psia]

Calculation Results

-- Emission Summary

Item Total HAPs Page 1	Uncontrolled [ton/yr] 42.970	Uncontrolled [lb/hr] 9.811	Controlled [ton/yr] 0.859	Controlled [lb/hr] 0.196 E&P TANK
Total HC	1628.953	371.907	32.579	7.438
VOCs, C2+	1595.030	364.162	31.901	7.283
VOCs, C3+	1436.371	327.939	28.727	6.559

Uncontrolled Recovery Info.

Vapor	70.4800	[MSCFD]
HC Vapor	70.2300	[MSCFD]
GOR	137.23	[SCF/bbl]

-- Emission Composition

No	Component	Uncontrolled [ton/vr]	Uncontrolled [lb/hr]	Controlled [ton/yr]	Controlled [lb/hr]
1 2 3 4 5 6 7 8 9	H2S 02 C02 N2 C1 C2 C3 i-C4 n-C4 i-C5	[ton/yr] 0.000 0.000 5.362 0.000 33.923 158.659 598.285 150.139 358.375 95.457	[lb/hr] 0.000 0.000 1.224 0.000 7.745 36.224 136.595 34.278 81.821 21.794	[ton/yr] 0.000 0.000 5.362 0.000 0.678 3.173 11.966 3.003 7.168 1.909	[1b/hr] 0.000 0.000 1.224 0.000 0.155 0.724 2.732 0.686 1.636 0.436
11 12 13 14 15 16 17 18 19	1-C5 n-C5 C6 C7 C8 C9 C10+ Benzene Toluene E-Benzene	81.363 40.222 56.611 8.686 2.547 1.718 3.945 5.436 0.196	18.576 9.183 12.925 1.983 0.582 0.392 0.901 1.241 0.045	1.627 0.804 1.132 0.174 0.051 0.034 0.079 0.109 0.004	0.372 0.184 0.258 0.040 0.012 0.008 0.018 0.025 0.001
20 21 22	Xylenes n-C6 224Trimethylp Total	2.055 28.820 2.517 1634.316	0.469 6.580 0.575 373.132	0.041 0.576 0.050 32.686	0.009 0.132 0.011 7.463

-- Stream Data

No. Component	MW	LP Oil	Flash Oil	sale Oil	Flash Gas	w&s	Gas
Total Emissions		mol % Page	mol % 2	mol %	mol %	mo1	%

RMR-S Snake Charmer	Draw Roger	Leo Fed	3875-20-29	-1FH 20150	520 EP Tanl	ks.txt
mol % 1 H2S	34.80	0.0000	0.0000	0.0000	0.0000	0.0000
0.0000	32.00	0.0000	0.0000	0.0000	0.0000	0.0000
0.0000 3 CO2	44.01	0.0453	0.0114	0.0000	0.7772	0.1334
0.3590 4 N2	28.01	0.0000	0.0000	0.0000	0.0000	0.0000
0.0000 5 C1	16.04	0.7862	0.0788	0.0000	16.0766	0.9188
6.2302 6 C2 15.5462	30.07	1.9621	0.8276	0.0003	26.4839	9.6462
7 C3 39.9755	44.10	5.1680	3.9022	0.1412	32.5274	43.9932
8 i-C4 7.6108	58.12	1.4954	1.3708	0.6122	4.1887	9.4568
9 n-C4 18.1668	58.12	5.3805	5.1348	3.5340	10.6917	22.1990
10 i-C5 3.8982	72.15	3.7862	3.8260	3.7700	2.9259	4.4226
11 n-C5 3.3226	72.15	4.5463	4.6384	4.7230	2.5559	3.7362
12 C6 1.4108	86.16	5.8584	6.0781	6.5007	1.1088	1.5738
13 C7 1.7196	100.20	22.1463	23.1099	25.0963	1.3189	1.9358
1.7190 14 C8 0.2306	114.23	9.6358	10.0737	10.9941	0.1702	0.2631
15 C9 0.0610	128.28	7.2007	7.5319	8.2318	0.0414	0.0716
16 C10+ 0.0333	152.16	16.2578	17.0089	18.6009	0.0219	0.0395
17 Benzene 0.1488	78.11	0.8710	0.9059	0.9753	0.1163	0.1664
18 Toluene 0.1739	92.13	3.7437	3.9108	4.2592	0.1313	0.1968
19 E-Benzene 0.0054	106.17	0.3641	0.3808	0.4159	0.0040	0.0062
20 Xylenes 0.0570	106.17	4.3996	4.6012	5.0267	0.0412	0.0655
21 n-C6 0.9853	86.18	5.2991	5.5087	5.9221	0.7690	1.1021
22 224Trimethylp 0.0649	114.24	1.0535	1.0999	1.1963	0.0499	0.0730
0.0013						
MW 48.15		98.65	101.30	105.94	41.30	51.85
Stream Mole Ratio 0.1262		1.0000	0.9558	0.8738	0.0442	0.0820
Heating Value 2718.16	[BTU/SCF]				2342.74	2920.67
Gas Gravity	[Gas/Air]				1.43	1.79
1.66 Bubble Pt. @ 100F	[psia]	51.19	20.89	5.65		
RVP @ 100F	[psia]	24.62	14.92	5.38		
Page 2					E&	P TANK
Spec. Gravity @ 100F		0.673	0.677	0.683		

RMR-S Snake Charmer Draw Roger Leo Fed 3875-20-29-1FH 20150520 EP Tanks.txt

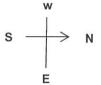
SM ENERGY CO. SITE SECURITY DIAGRAM:

WELL NO: ROGER LEO FED 3875-20-29-1FH LEASE NO: WYW181101 & WYW180165 FIELD NAME: SNAKE CHARMER DRAW FIELD LOCATION: NENE SEC 20-T38N-R75W COUNTY: CONVERSE CO. STATE: WY

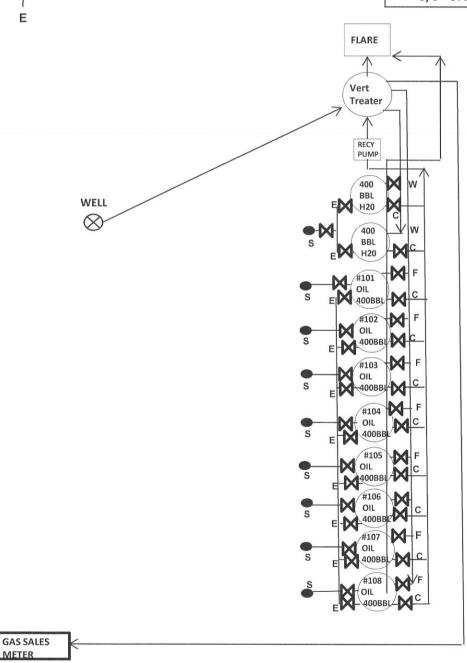
SITE FACILITY PLAN LOCATED AT: SM ENERGY CO 550 N 31ST ST, SUITE 500 BILLINGS, MT 59103

SEALING	PRODUCTION OR NORMAL OPERATIONS	RECYCLING	SALES
C=RECYCLING	o/c	0	sc
E=EQUALIZER	o/c	O/C	sc
F=PRODUCTION	0	O/C	sc
I=INJECTION	sc	SC	0

WHERE: O - OPEN, SO - SEALED OPEN, C - CLOSED, SC - SEALED CLOSED, O/C - OPEN OR SEALED



NOT TO SCALE



METER

), w

QUESTAR APPLIED TECHNOLOGY

1210 D. Street, Rock Springs, Wyoming 82901 (307) 352-7292

2:33 PM

LIMS ID: Analysis Date/Time: N/AS 4/6/2015 Description: Field:

Allemand 12-2

Analysis Date/Time Analyst Initials: Instrument ID:

4/6/20 PRP Field: ML#: Allemand SM Energy Quesbtex

Data File:

Instrument 1 QPC24.D GC Method: GPA 2286

Date Sampled:

4/1/2015

Component	Мо	1%	V	Vt%	LV%
Methane	76.8150		56.5749		67.0104
Ethane	12.0607		16.6496		16.6456
Propane	5.6270		11.3916		7.9849
Isobutane	0.6785		1.8106		1.1431
n-Butane	1.5859		4.2318		2.5748
Neopentane	0.0122		0.0405		0.0241
Isopentane	0.4212		1.3950		0.7939
n-Pentane	0.3867		1.2809		0.7213
2,2-Dimethylbutane	0.0048		0.0190		0.0103
2,3-Dimethylbutane	0.0363		0.1436		0.0766
2-Methylpentane	0.0872		0.3450		0.1863
3-Methylpentane	0.0535		0.2116		0.1124
n-Hexane	0.1200		0.4748		0.2541
Heptanes	0.3889		1.7036		0.7990
Octanes	0.0717		0.3752		0.1847
Nonanes	0.0836		0.4546		0.2082
Decanes plus	0.0261		0.1704		0.0825
Nitrogen	0.5252		0.6754		0.2965
Carbon Dioxide	1.0155		2.0519		0.8913
Oxygen	0.0000		0.0000		0.0000
Hydrogen Sulfide	0.0000		0.0000		0.0000
Total	100.0000		100.0000		100.0000
Global Properties		Units			
Gross BTU/Real CF	1293.0			t 60°F and14	•
Sat.Gross BTU/Real CF	1269.9		BTU/SCF at	t 60°F and14	.73 psia
Gas Compressibility (Z)	0.9961				
Specific Gravity	0.7528		air=1		
Avg Molecular Weight	21.782		gm/mole		
Propane GPM	1.542151		gal/MCF		
Butane GPM	0.720159		gal/MCF		
Gasoline GPM	0.582910		gal/MCF		
26# Gasoline GPM	1.090623		gal/MCF		
Total GPM	6.376388		gal/MCF		
Base Mol%	99.534		%v/v		
Sample Temperature:	66		°F		
Sample Pressure:	28		psig		
H2SLength of Stain Tube	e N/A		ppm		

Component	Mol%	Wt%	LV%
Benzene	0.0176	0.0632	0.0254
Toluene	0.0433	0.1833	0.0747
Ethylbenzene	0.0034	0.0165	0.0067
M&P Xylene	0.0273	0.1333	0.0545
O-Xylene	0.0071	0.0348	0.0140
2,2,4-Trimethylpentane	0.0106	0.0557	0.0275
Cyclopentane	0.0000	0.0000	0.0000
Cyclohexane	0.0757	0.2925	0.1327
Methylcyclohexane	0.0947	0.4271	0.1961
Description:	Allemand 12-2		

GRI GlyCalc Information

Component	Mol%	Wt%	LV%
Carbon Dioxide	1.0155	2.0519	0.8913
Hydrogen Sulfide	0.0000	0.0000	0.0000
Nitrogen	0.5252	0.6754	0.2965
Methane	76.8150	56.5749	67.0104
Ethane	12.0607	16.6496	16.6456
Propane	5.6270	11.3916	7.9849
Isobutane	0.6785	1.8106	1.1431
n-Butane	1.5859	4.2318	2.5748
Isopentane	0.4334	1.4355	0.8180
n-Pentane	0.3867	1.2809	0.7213
Cyclopentane	0.0000	0.0000	0.0000
n-Hexane	0.1200	0.4748	0.2541
Cyclohexane	0.0757	0.2925	0.1327
Other Hexanes	0.1818	0.7192	0.3856
Heptanes	0.1470	0.6818	0.3426
Methylcyclohexane	0.0947	0.4271	0.1961
2,2,4 Trimethylpentane	0.0106	0.0557	0.0275
Benzene	0.0176	0.0632	0.0254
Toluene	0.0433	0.1833	0.0747
Ethylbenzene	0.0034	0.0165	0.0067
Xylenes	0.0344	0.1681	0.0685
C8+ Heavies	0.1436	0.8156	0.4002
Subtotal	100.0000	100.0000	100.0000
Oxygen	0.0000	0.0000	0.0000
Total	100.0000	100.0000	100.0000

QUESTAR APPLIED TECHNOLOGY

1210 D. Street, Rock Springs, Wyoming 82901 (307) 352-7292

7:10 AM

LIMS ID: N/A
Analysis Date/Time: 4/7/2015
Analyst Initials: PRP
Sample Temperature: 66
Sample Pressure: 28
Date Sampled: 4/1/2015

Description: Allemand 12-2
Field: Allemand
ML#: SM Energy
GC Method: Quesliql GPA 2186

Data File: QPC31.D Instrument ID: 1

Component	Mol%	Wt%	LV%
Methane	0.7862	0.1270	0.2996
Ethane	1.9621	0.5939	1.1800
Propane	5.1680	2.2941	3.2016
Isobutane	1.4954	0.8750	1.1004
n-Butane	5.3805	3.1482	3.8143
Neopentane	0.0379	0.0276	0.0327
Isopentane	3.7483	2.7225	3.0825
n-Pentane	4.5463	3.3020	3.7057
2,2-Dimethylbutane	0.1086	0.0942	0.1019
2,3-Dimethylbutane	1.1298	0.9801	1.0412
2-Methylpentane	2.9119	2.5262	2.7179
3-Methylpentane	1.7081	1.4818	1.5676
n-Hexane	5.2991	4.5971	4.9002
Heptanes	23.0173	22.3981	21.5425
Octanes	14.4330	15.7297	14.8370
Nonanes	11.9644	14.3886	13.2530
Decanes plus	16.2578	24.6941	23.6045
Nitrogen	0.0000	0.0000	0.0000
Carbon Dioxide	0.0453	0.0201	0.0174
Total	100.0000	100.0000	100.0000

Global Properties

Units

Avg Molecular Weight	99.3356 gm	n/mole
Pseudocritical Pressure	450.09 ps	ia
Pseudocritical Temperatu	500.98 de	gF
Specific Gravity	0.70785 gm	n/ml
Liquid Density	5.9011 lb/	gal
Liquid Density	247.85 lb/	bbl
Specific Gravity	2.9053 air	=1
SCF/bbl	950.61 SC	F/bbl
SCF/gal	22.6335 SC	F/gal
MCF/gal	0.0226 MG	CF/gal
gal/MCF	44.198 ga	I/MCF
Net Heating Value	4917.7 BT	U/SCF at 60°F
Net Heating Value	18893.2 BT	U/lb at 60°F
Gross Heating Value	5349.2 BT	U/SCF at 60°F
Gross Heating Value	20325.9 BT	U/lb at 60°F
Gross Heating Value	121411.7 BT	U/gal at 60°F
API Gravity	68.4	
MON	63.2	
RON	65.0	
RVP	72.025 ps	ia

Component	Mol%	Wt%	LV%
Benzene	0.8710	0.6849	0.5480
Toluene	3.7437	3.4726	2.8190
Ethylbenzene	0.3641	0.3891	0.3160
M&P Xylene	3.3257	3.5544	2.8958
O-Xylene	1.0739	1.1477	0.9183
2,2,4-Trimethylpentane	1.0535	1.2114	1.1906

Data File:

Allemand 12-2

Page #2

GRI E&P TANK INFORI	MATION		
Component	Mol%	Wt%	LV%
H2S	0.0000	0.0000	0.0000
O2	0.0000	0.0000	0.0000
CO2	0.0453	0.0201	0.0174
N2	0.0000	0.0000	0.0000
C1	0.7862	0.1270	0.2996
C2	1.9621	0.5939	1.1800
C3	5.1680	2.2941	3.2016
IC4	1.4954	0.8750	1.1004
NC4	5.3805	3.1482	3.8143
IC5	3.7862	2.7501	3.1152
NC5	4.5463	3.3020	3.7057
Hexanes	5.8584	5.0823	5.4286
Heptanes	22.1463	21.7132	20.9945
Octanes	9.6358	11.0457	10.8274
Nonanes	7.2007	9.2974	9.1229
Benzene	0.8710	0.6849	0.5480
Toluene	3.7437	3.4726	2.8190
E-Benzene	0.3641	0.3891	0.3160
Xylene	4.3996	4.7021	3.8141
n-C6	5.2991	4.5971	4.9002
2,2,4-Trimethylpentane	1.0535	1.2114	1.1906
C10 Plus			
C10 Mole %	16.2578	24.6941	23.6045
Molecular Wt.	152.1604		
Specific Gravity	0.7409		
Total	100.00	100.00	100.00

1210 D Street Rock Springs, Wy. 82901 Ph: 307-352-7292

Fax: 307-352-7326

Questar Energy Services Applied Technology Services

API Gravity Reid Vapor Pressure

Producer:

SM Energy

Well Name:

Allemand 12-2

Tank Number:

4

Tank Temp *F:

46*

Field:

Wildcat

County and State:

Converse, WY

Corrected API Gravity: 43.9 @ 60*F

RVP

5.4#

Date Sampled:

4/1/15

Date Analyzed:

4/6/15

Sampled By:

Drebin

Analyzed By:

Putnam

i , .

Questar Applied Technology Services

1210 D Street Rock Springs, Wyoming 82902 Phone: (307) 352-7292 Fax: (307) 352-7326

WATER ANALYSIS REPORT

COMPANY:

SM Energy

FIELD:

Allemand Converse

COUNTY: STATE:

Wyoming

WELL:

Allemand 12-2

FORMATION:

SAMPLE POINT:

H20 Dump Valve

TYPE OF WATER: Produced

DATE SAMPLED: 4-1-15 DATE ANALYZED: 4-10-15

ANALYZED BY:

Putnam

SAMPLED BY:

Dreben

DISSOLVED SOLIDS	mg / L
CATIONS:	
Sodium, Na:	10,212
Calcium, Ca:	704
Magnesium, Mg:	423
Barium, Ba:	N/A
ANIONS:	
Chloride, CI:	18,000
Sulfate, SO ₄ :	0
Carbonate, CO₄:	0
Bicarbonate, HCO₄:	400
Iron, Fe:	25
Sulfide, H ₂ S:	N/A
TOTAL DISSOLVED:	29,764
OTHER PROPERTIES:	
pH:	6.85
Specific Gravity, 60/60F:	1.0262
Resistivity: (ohms/meter)	0.208
Sample Temperature:	71*F
REMARKS & RECOMME	NDATIONS:

SMA Daily Estimated Production History

Region: Billings Bus Area: S Rockies Gillette

Route: BILWY01 Facility: ROGER LEO FED 3875-2029-1FH - FACILITY COMP: ROGER LEO FED 3875-2029-1FH [#11512687-000]

State: Wyoming
Prospect: DEEP POWDER /
CONVERSE WY
Operator: SM ENERGY COMPANY

County: CONVERSE Field: SNAKE CHARMER DRAW Prod Stat: Producing

Displaying Prod Estimates for 2 months ending 5/16/2015.

Treater	Trtr Pres	63	_	84 135		92 150	81 148	0 100	74 125	96 135																							•	13	13	13	133	13	13	13
Spec Grav	WH Mtr																																							
API	0				39.3	39.3	39.3	39.5	39.3		40.8	40.0	39.7	39.5	39.3	39.3	39.8	40.5	40.7	40.4	40.0	39.9	40.0	39.3	40.1	40.7		40.8	40.5	39.3	39.3	30.0	39.8	39.6	39.3	40.1	40.7		39.3	39.3
Fluid	Level																																							
(Psia)	Csd	350																														0000	0.000							
Pressure (Psia)	Tbg	-	1450	1080	1120	1020	1000	1000	1100	1020	930	890	950	940	780	750	725	700	850	680	680	069	680	650	620	009	1150	1300	220	009	240	0 000	400	410	460	450	310	350	000	325
	Choke	0	0	~	~	~	_	~	~	-	1	-	-	Υ-	-	Υ-	-	_	0	-	-	τ-	_	-	~	-	-	Ψ	-	-	-		1	· ~	.	-	-	-		-
DownTime	Dn Reason	24 WORKOVER	16 WORKOVER	0	0	0	0	3 Wellhead Problems	11 Wellhead Problems	7 Wellhead Problems	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	5 High SW Tank Level	14 Other Weather	0	0	0	3	, 0	0	0	0	0	0		0
Hrs		1	8	24	24	24	24	21	13	17	24	24	24	24	24	24	24	24	24	24	24	24	24	24	24	24					24		24	24	24	24	24	24		24
-	Water	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0		0 0	0	0	0	0	0	0		0
Injection	Gas V																															c	>							
S	Vent	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	0	00.0	00	0	0	0	0	0		0
Lease Use Gas	Fuel	0	0	0	0	0	30	0	30	30	30	30	30	30	30	30	30	30	30	30	30	30	30	30	30	30	30	15	30	30	30	201	30	300	30	29	29	30		29
Lease	Flare	0	188	603	528	835	265	38	218	96	16	0	0	0	52	0	180	181	99	104	173	0	0	15	42	0	0	0	0	12	2002	1000	0	89	78	0	0	98		0
_	Gas	0	512	818	1154	868	1328	138	999	1787	1666	1685	1574	1722	1483	1634	1200	1465	1169	801	1474	1144	1239	1105	1151	1255	1075	260	1368	1266	1275	1183	1330	1227	1252	1278	1244	1022		526
Sales	lio	0	0	0	1198	472	682	1430	473	0	1448	1685	963	1456	719	1200	1205	927	1260	239	963	952	1197	718	922	974	0	672	953	952	946		954	949	702	942	943	723		969
C	1CF	0	700	1421	1682	1733	1623	176	913	1913										935	1677			1150	1223	1285	1105	275	1398	1308	1310		1360	1325	1360	1307	1273	1147		555
NOI	Gas MCF					200	_																																	
PRODUCTION	Wtr BBL	0	2085	3060	2935	2805	2430	245	1510	2595	1660	1905	1650	1630	1540	1270	1400	1300	895	841	2599	1414	433	0	206	846	718	84	779	758	815	1203	894	883	872	785	661	741		735
Prod PRODUCTION Sales	Oil BBL	0	260	805	1028	785	1219	77	585	1294	1143	1109	1053	1201	1020	1110	1187	862	872	655	1009	870	994	825	865	825	711	171	946	839	846	40407	892	893	877	885	1062	826		447
Prod	ا ق	۵	כ	D	\supset	⊃	⊃	\supset	⊃	⊃	⊃	⊃	ם	⊃	\Box	⊃	n	コ	\supset	ח	⊃	⊃	⊃	⊃	⊃	⊃	D	D	D	⊃	D	67	-) D)))	ם	ם		>
	Leak	ட	ш	F	щ	L	ш	ш	ட	Щ	щ	ш	Щ	ш	ш	ш	ш	ш	Щ	ш	ш	ш	Щ	ш	Щ	ш	ட	ш	ш	L	ц.		ш	. ц.	ш	ட	Щ	ш		ш
200	Prod Dt	04/1/2015	04/2/2015	04/3/2015	04/4/2015	04/5/2015	04/6/2015	04/7/2015	04/8/2015	04/9/2015	04/10/2015	04/11/2015	04/12/2015	04/13/2015	04/14/2015	04/15/2015	04/16/2015	04/17/2015	04/18/2015	04/19/2015	04/20/2015	04/21/2015	04/22/2015	04/23/2015	04/24/2015	04/25/2015	04/26/2015	04/27/2015	04/28/2015	04/29/2015	04/30/2015	Prod Dy Ave:	05/1/2015	05/2/2015	05/3/2015	05/4/2015	05/5/2015	05/6/2015	710001	05/1/2015

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130	80	125	125	125	125	125		125.0
70	0	06	06	52	50	50		9.79
		41.1	40.7	39.7		39.3		39.9
350	1160	550	430	490	510	530		464.1
-	-	-	~	0	0	0		
24 Other Weather	24 Other Weather	2 Other Weather	0	0	0	0	29	4
0	0	23	24	24	24	24	318	20
0	0	0	0	0	0	0	0	0
								0
0	0	0	0	0	0	0	00.0	0
0	0	28	30	30	29	29	394	28
0	2	0	936	140	0	0	1319	94
0	116	850	119	466	456	661	11956	854
0	0	720	725	928	0	929	10177	727
0	118	878	1085	636	485	069	13669	926
440	0	246	664	340	293	387	8623	616
0	0	826	827	479	333	476	9650	689
۵	Q	⊃	⊃	ם	\supset	_	14	
ш	ш	ш	ட	ш	ш	ட	0	
05/10/2015	05/11/2015	05/12/2015	05/13/2015	05/14/2015	05/15/2015	05/16/2015	Monthly Total:	Prod Dy Avg:

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